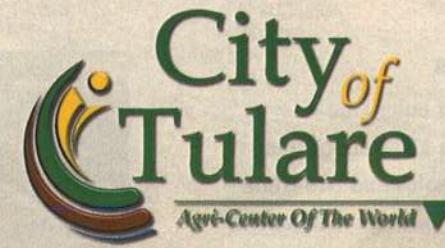


Plant Characteristics

| Items | Characteristics | Items | Characteristics |
|--|--------------------|---|-----------------|
| Design Flows | | | |
| Influent Flow | 6.00 mgd | Process Air Requirement | 3,100 scfm |
| Internal Recycle Flows | 0.09 mgd | Design Peaking Factor | 1.3 |
| Total Primary Influent Flow | 6.09 mgd | Peak Process Air Requirement | 4,030 scfm |
| Primary Clarifiers | | | |
| Number | 4 | Other Uses (Channel Air, etc.) | 500 scfm |
| Dimensions, LxWxD, FTxFTxFT | 80x18.5x9.5 | Total Design Air Requirement | 4,530 scfm |
| Total Surface Area | 5,920 sf | Secondary Clarifiers | |
| Surface Overflow Rate | 1,028 gpd/sf | Number | 6 |
| TSS Removal (Percent) | 59 | Dimensions, LxWxD, FTxFTxFT | 95x18.5x13.2 |
| BOD Removal (Percent) | 25 | Total Surface Area | 10,545 sf |
| Primary Sludge | | | |
| Total Solids | 9,681 ppd | Surface Overflow Rate | 565 gpd/sf |
| Concentration | 50,000 mg/L | Waste Activated Sludge | |
| Flow | 0.023 mgd | Total Solids | 6,711 ppd |
| Primary Effluent Bypass | | | |
| Flow Bypassed Around Biofilter (Percent) | 0-50 | Concentration | 7,891 mg/L |
| Biofilters | | | |
| Number | 2 | Flow | 0.102 mgd |
| Dimensions, LxWxD, FTxFTxFT | 44x44x14 | Gravity Belt Thickener | |
| Total Volume | 54,208 cf | Number | 1 |
| Organic Loading, ppd BOD/1,000 cf | 87 | Belt Size, M | 2 |
| Anoxic Basin | | | |
| Total Volume | 0.645 MG | Solids Loading | 2,500 lb/hr |
| Number of Zones | 6 | Feed Rate | 500 gpm |
| Zone 1 Volume | 0.073 MG (anoxic) | Operating Cycle, Days/Week | 5 |
| Zone 2 Volume | 0.073 MG (anoxic) | Operating Cycle, Hours/Day | 4 |
| Zone 3 Volume | 0.073 MG (anoxic) | Thickening Solids Concentration, (Percent) | 5.0 |
| Zone 4 Volume | 0.103 MG (aerobic) | Solids Capture, (Percent) | 90 |
| Zone 5 Volume | 0.161 MG (aerobic) | Waste Activated Sludge | |
| Zone 6 Volume | 0.161 MG (aerobic) | Total Solids | 15,720 ppd |
| Aeration Basins | | | |
| Number of Basins | 3 | Volatile Solids | 12,610 ppd |
| Volume, Each Basin | 0.26 MG | Flow | 0.038 mgd |
| Total Aeration Basin Volume | 0.78 MG | Anaerobic Digesters | |
| Activated Sludge Criteria | | | |
| SRT | 4.8 days | Number | 2 |
| MLSS | 2,800 mg/L | Diameter | 65 ft |
| Effluent, NH ₃ | 0.6 mg/L | Side Water Depth | 18 ft |
| Effluent, NO ₃ | 6.5 mg/L | Effective Total Volume (5 Percent Grit Allowance) | 113 |
| Effluent, NO ₃ | <10.0 mg/L | Volatile Solids Loading, ppd VS/1000 cf | 0.11 |
| | | Hydraulic Retention Time, Days | 23 |
| | | Percent Destruction | 49 |



June 2006



Domestic Wastewater Treatment Plant Nitrogen Removal Upgrade Project

Contact Information

City of Tulare
 Water Pollution Control Facilities
 Richard Bono, Superintendent
 1875 S. West Street
 Tulare, CA 93274
 Office 559-685-2360
 Fax 559-685-8688
 www.ci.tulare.ca.us



Plant Processes



A Headworks

Raw wastewater enters the headworks from a system of interconnected manholes and two trunk sewers. It flows through mechanical bar screens removing rags, stick, and other objects that may clog pumps and pipes throughout the plant.

B Grit Removal

Wastewater enters the grit unit where the grit settles to the bottom. A mechanical scraping system conveys the settled grit to a hopper which is then hauled to a landfill.

C Primary Sedimentation

Flow is then directed to the primary sedimentation basin where settleable and floatable materials are removed and pumped to the digesters. The effluent can then be sent to the biotowers or bypassed to the anoxic basins.



Biotowers

D Biotowers

The flow entering the two biological towers, referred to as biotowers, is sprayed down over a redwood media which provides a surface for microorganisms to grow and feed. This process removes the organics from the wastewater.



Anoxic Basin

E Anoxic Basins

Once through the biotowers the flow enters the anoxic basins. In these basins the removal of nitrogen from the wastewater takes place. This process is referred to as denitrification. Returned Activated Sludge (RAS) can be pumped to the basins along with the primary effluent bypass.



Aeration Basins

F Aeration Basins

Once through the anoxic basin the wastewater enters the aeration basins. Fine bubble diffusers introduce air, providing oxygen for the microorganisms helping in the activated sludge process. These organisms break down and consume the organic material in the wastewater.

G Blowers

Blowers provide necessary air for the plant's biological processes and air to mix wastewater channels.

H Secondary Sedimentation

As the flows enter the secondary sedimentation basins from the aeration basins, solids settle to the tank bottom. The settled material is pumped back to the anoxic basins and the excess settled material is pumped to the solids thickener.

I Pump Gallery

Return pumps, waste pumps, sump pumps and other plant utilities are located in the pipe and pump gallery.

J Effluent Pump Station

The secondary effluent pump station lifts the domestic plant effluent to storage ponds for subsequent farm irrigation.

K Solids Thickeners

The Gravity Belt Thickener receives sludge from the sedimentation basins. The thickeners decrease the water content of the sludge by spreading a sludge and polymer mixture on a porous belt.



Digesters

L Digesters

Thickened biosolids and primary sludge are pumped to two anaerobic digesters which stabilize the biosolids to prevent odors and disease. Methane gas produced during the digestion process is used to heat the digesters.

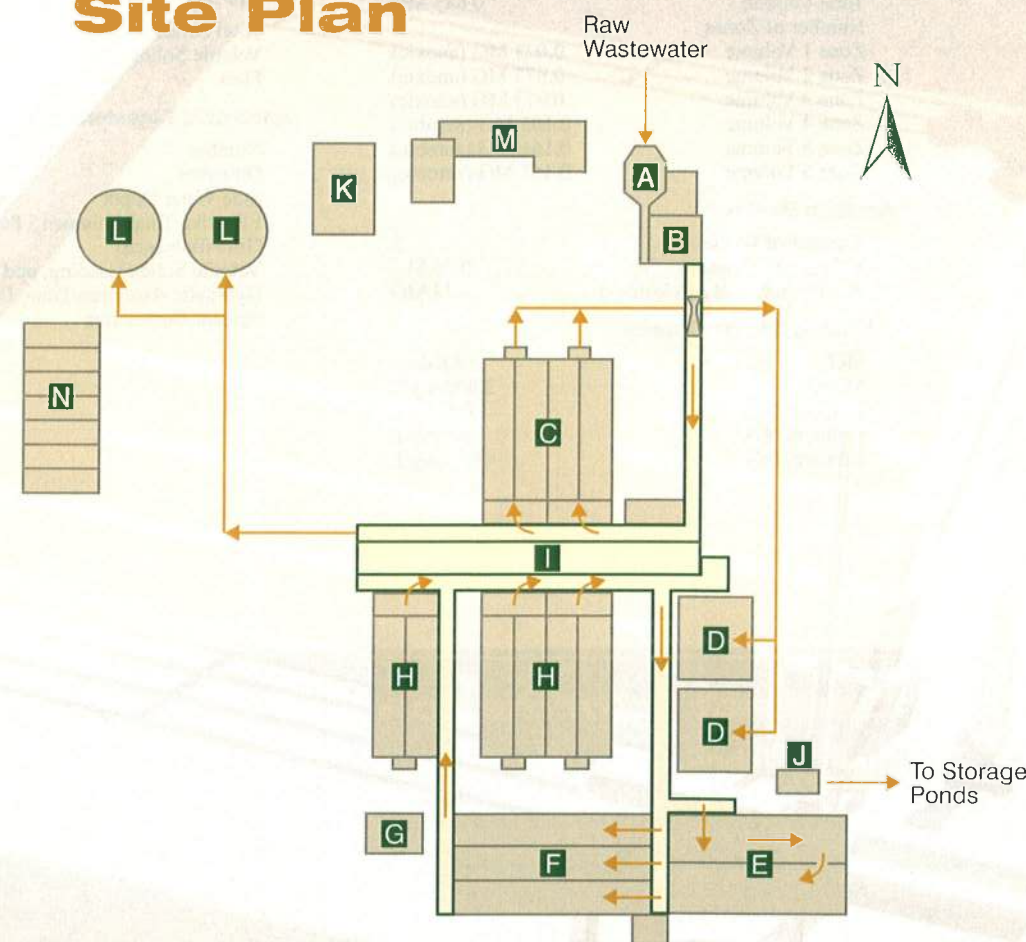
M Operations Building and Laboratory

The operations building houses the main plant controls and laboratory. The treatment processes are continuously monitored by a computer control system. The final reclaimed wastewater is monitored prior to farm irrigation to assure compliance with State requirements.

N Sludge Drying Beds

Sludge beds provide an area for storage and drying of digested biosolids. Dried biosolids can be spread on city-owned farmland.

Site Plan



The City of Tulare Water Pollution Control Facility (TWPCF) is located southwest of the City. The facility consists of two separate wastewater treatment processes: an activated biofilter/activated sludge plant for treating domestic wastewater, and a Bulk Volume Fermenter (BVF) anaerobic reactor plant for treatment of the industrial wastewater.

The Domestic Plant can treat 6.0 million gallons per day (mgd) of wastewater. The secondary treatment plant's goal is to remove the organic and solid material and the nitrogen in the wastewater that can pollute the environment.

Tulare's first treatment facility was built in the 1920's. Waste was given minimal treatment and used to irrigate crops. As the town and industry grew, additional treatment was required. Several major improvements have been made in the past 30 years to help handle these needs.

The recent expansion in 2006 added an anoxic basin to help in the removal of nitrogen to meet the City's total nitrogen requirements.